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# RADIATING, CONVECTING AND CONDUCTING FINS: NUMERICAL AND LINEARIZED SOLUTIONS

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#### **NOMENCLATURE**

- area of fin cross section: A,
- circumference of fin cross section; **C**,
- heat-transfer coefficient; h,
- k, thermal conductivity of fin;
- L, fin length:
- convection parameter, equation (1a);
- N, radiation parameter, equation (1a);
- Q, T, rate of heat loss from fin;
- temperature;
- X, dimensionless coordinate, x/L;
- coordinate measuring axial distance along fin (x = 0 is fin base).

#### Greek symbols

- emittance of fin surface; €,
- fin effectiveness, equation (2); η,
- temperature ratio,  $T/T_h$ ; θ.
- Stefan-Boltzmann constant. σ.

# Subscripts

- fin base: b.
- fluid bulk. α.

## Superscript

effective radiation environment.

# INTRODUCTION

THE PURPOSE of this note is to provide representative results for one-dimensional heat conduction in fins of axially unchanging cross section, the surface heat transfer involving both convection and radiation. The governing energy equation is

$$d^2\theta/dX^2 = N_r(\theta^4 - \theta^{*4}) + N_{co}(\theta - \theta_{\infty})$$
 (1)

$$\theta = \frac{T}{T_b}, \qquad X = \frac{x}{L}, \qquad N_r = \frac{\epsilon \sigma T_b^3 C L^2}{kA}, \qquad N_{cv} = \frac{hC L^2}{kA},$$

$$\theta^* = \frac{T^*}{T_c}, \qquad \theta_\infty = \frac{T_\infty}{T_c} \qquad (1a)$$

in which  $T_b$ ,  $T_\infty$ , and  $T^*$  are, respectively, the temperatures at the fin base, in the adjacent fluid, and of the effective radiation environment.‡ The area and circumference of the cross section are A and C; while L is the length of the fin. Equation (1) is to be solved subject to the boundary conditions  $\theta(0) = 1$  and  $(d\theta/dX)_1 = 0$ , and for specified values of the four independent parameters  $N_n N_{cm} \theta^*$ , and  $\theta_m$ .

In addition to direct numerical solutions, linearized

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The absorbed radiant energy per unit time and area is  $\epsilon \sigma T^{*4}$ .

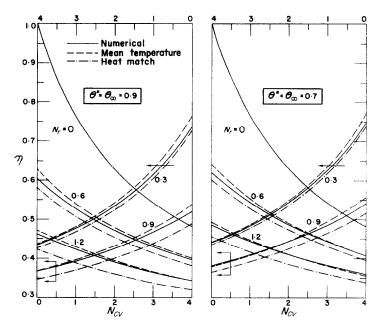


Fig. 1. Effectiveness of convecting and radiating fins,  $\theta^* = \theta_\infty = 0.9$  and 0.7.

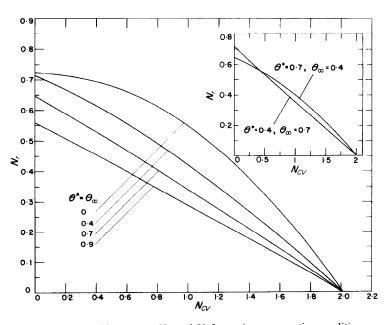


Fig. 2. Rélationship between  $N_{cv}$  and  $N_r$  for optimum operating conditions.

solutions have also been obtained by letting  $\theta^4 = \theta \tilde{\theta}^3$ , where  $\tilde{\theta}$  is independent of x. The linearization constant  $\tilde{\theta}$  was determined by two alternative approaches. In the first method (termed the heat match), one uses the linearized solution to evaluate the heat conduction  $Q_\epsilon$  at the fin base and the overall heat loss  $Q_l$  by convection and radiation from the surfaces of the fin, the radiation involving fourth-power emission. For an exact solution,  $Q_\epsilon$  and  $Q_l$  are necessarily equal; for the linearized solution, the condition  $Q_\epsilon = Q_l$  provides a means for determining  $\tilde{\theta}$ . In the second method (mean temperature method),  $\tilde{\theta}$  is determined as the average of the  $\theta$  values at x = 0 and x = L.

The fin heat transfer can be expressed in terms of the effectiveness as

$$\eta = \frac{Q}{Q_{\text{ideal}}} = \frac{-kA(dT/dx)_0}{CL[\epsilon\sigma(T_b^4 - T^{*4}) + h(T_b - T_\infty)]}$$
(2)

where the ideal fin is one of infinite thermal conductivity.

The presence of four independent parameters coupled with journal space limitations restricts the presentation of results to a few representative cases. Figure 1 shows a plot of fin effectiveness as a function of  $N_{cv}$  for parametric values of  $N_r$ , with  $\theta^* = \theta_\infty = 0.9$  and 0.7. The solid lines correspond to the numerical solutions, while the dashed and dot-dashed lines are for the linearized solutions. The uppermost curve  $(N_r = 0)$  in each graph is for purely convective heat loss, while the ordinate intercepts  $(N_{cv} = 0)$  correspond to purely radiative heat loss.

For given values of  $N_r$  and  $N_{cv}$ , the fin effectiveness corresponding to simultaneous radiative and convective loss is seen to be lower than either of the respective  $\eta$  values for purely radiative and purely convective heat loss. Moreover, while  $\eta$  decreases with increasing values of  $N_r$  and  $N_{cv}$ , as for the respective cases of pure radiation and pure convection, the rate of decrease is markedly influenced by the simultaneous action of the two transport mechanisms. At low  $N_r$  (small radiation contribution),  $\eta$  decreases rapidly

with  $N_{cv}$ . On the other hand, at larger  $N_r$ ,  $\eta$  is much less sensitive to increases in  $N_{cv}$ . Similarly,  $\eta$  becomes less sensitive to  $N_r$ , when  $N_{cv}$  is large. Within the range of the figure,  $\eta$  is not a strong function of the specific values of  $\theta^*$  and  $\theta_{cv}$ .

It is also seen from Fig. 1 that the accuracy of the results based on the mean temperature model is generally very good, being within that required for design.

Consideration is now given to the so-called optimum fin, for which the heat transfer per unit volume of fin is a maximum. The determination of the optimum condition depends on the specifics of the fin cross section. Numerical results will be derived here for the straight fin of rectangular profile (thickness t). If the fin width is fixed, the optimum is found by regarding the profile area  $A_p$  (= Lt) as a constant and varying either L or t until the maximum heat transfer is encountered. In the numerical determination of the optimal condition, it is especially advantageous to use the linearized models since the relevant partial derivatives can be evaluated from closed form expressions. In view of its relative simplicity, the mean temperature model was employed.

The optimum fin results are shown in Fig. 2. The main portion of the figure corresponds to cases where  $\theta^* = \theta_{\infty}$ , while the inset shows a few cases for which  $\theta^* \neq \theta_{\infty}$ . The ordinate intercepts are the  $N_r$  values defining optimum conditions for purely radiating fins, while the abscissa intercept (2.0142) is the optimum condition for purely convecting fins.

The figure shows that for simultaneous radiative and convective heat loss, the  $N_r$ ,  $N_{cv}$  values defining the optimum are always less than are those when these processes act separately. In other words, the optimum  $N_r$  decreases with increasing  $N_{cv}$ , and the optimum  $N_{cv}$  decreases with increasing  $N_r$ . Once the optimum  $N_r$ ,  $N_{cv}$  are known, then the ratio  $N_r/N_{cv}$  yields the corresponding value of  $\epsilon \sigma T_b^3/h$ . The fin effectivenesses  $\eta$  that correspond to the optimum  $N_r$ ,  $N_{cv}$  of Fig. 2 generally fall in the neighborhood of 0·6.